

# Hydromagnetic Boundary Layer Slip Flow and Heat Transfer with Thermal Radiation and Viscous Dissipation

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**Abstract** – The simultaneous effects of radiation and viscous dissipation on heat transfer over a moving sheet with slip in both velocity and boundary condition has been numerically analyzed. The governing boundary layer equations are formulated and transformed into ordinary differential equations using similarity transformation. The resulting ordinary differential equations are solved numerically using the Runge-Kutta fourth order algorithm coupled with a shooting technique. Numerical computations are performed for pertinent values of the physical parameters involved. For illustration of the results, numerical values are plotted in graphical form and discussed quantitatively with respect to the influence of governing physical parameters, namely, magnetic field parameter  $M$ , Eckert number  $Ec$ , Biot Number  $Bi$ , Injection/Suction parameter  $f_w$ , Radiation Parameter  $R$  and slip parameter  $\beta$ . The Prandtl number of the based fluid (water) is kept constant at 6.2. It is noted that the magnetic parameter slackens the fluid motion whilst increasing it temperature and skin friction coefficient.

**Keywords** – Boundary Layer, Heat Transfer, Radiation, Slip Flow, Viscous Dissipation.

## I. INTRODUCTION

The problem on boundary layer flow of an electrically conducting fluid in the presence of magnetic field has a varied range of applications in many engineering problems namely; MHD generators, in the polymer industry, nuclear reactors, geothermal energy extraction among others. The flow and radiative heat transfer characteristics induced by a continuously moving surface are of a great significance in many engineering applications. This is because the quality of the final product depends on the rate of heat transfer of the ambient fluid particles and the magnetic field intensity. Experimental and theoretical investigations on conventional electrically conducting fluids indicate that magnetic field changes the transport and heat characteristics of conventional fluids. The problem on steady boundary layer flow due to a continuously moving surface was first studied by Sakiadis [1]. Thereafter, several authors [2]-[6] extended the study of the same problem for various aspects for both Newtonian and non-Newtonian fluids.

The effect of thermal radiation on heat transfer processes is very significant at high operating temperatures and as a result it has many engineering applications. In recent times, many researchers have included the effect of thermal radiation in their work.

Makinde [7] studied the effect of thermal radiation and mass transfer past a moving vertical porous plate. Sajid and Hayat [8] showed the influence of thermal radiation on the flow over an exponentially stretching sheet and they solved the problem analytically using the homotopy analysis method. K Das [9] examined the impact of thermal radiation on MHD slip flow over a flat plate with variable fluid properties. Motsumi and Makinde. [10] studied the effects of thermal radiation and viscous dissipation on boundary layer flow of nanofluids over a permeable moving flat plate. Several other authors [11]-[14] have studied the effect of thermal radiation under different conditions. The main purpose of the present study is to investigate the combined effects of hydro magnetic boundary layer slip flow and heat transfer with thermal radiation and viscous dissipation on a horizontal moving plate surface. In subsequent sections of this paper we will have a formulation of the model governing equations, and then we will reduce the model governing equations to a dimensionless form. Thereafter we will use a Maple computer programme to get our results which is presented in graphical and tabular form. We then have a discussion where the graphical representation of the pertinent parameters on the flow field and heat transfer characteristics is displayed and discussed in detail.

## II. MATHEMATICAL FORMULATION OF THE PROBLEM

Consider the steady laminar incompressible two dimensional boundary layer flow of an electrically conducting fluid flowing past a highly lubricated surface. We choose the coordinate system such that x-axis is along the horizontal plate and y-axis is orthogonal to the plate. The physical flow model and coordinate system is shown in Fig. 1 below. A transverse magnetic field of strength  $B_0$  is applied parallel to the y-axis. The variable plate surface permeability function is defined by  $V_0 = -f_w(av_f)^{1/2}$  where  $f_w$  is the suction/injection parameter; with  $f_w > 0$  representing the transpiration rate at the plate surface,  $f_w < 0$  corresponds to injection and  $f_w = 0$  for an impermeable surface.

Considering the fluid as a continuous media with thermal equilibrium and slip occurring between the base fluid and the solid particles, the basic steady governing

equations of continuity, momentum and thermal energy are given respectively as;

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho_f} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2}{\rho_f} \quad (2)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} + \frac{\mu}{(\rho C_p)_f} \left[ \frac{\partial u}{\partial y} \right]^2 + \frac{\sigma B_0^2 u^2}{(\rho C_p)_f} - \frac{1}{(\rho C_p)_f} \frac{\partial q_r}{\partial y} \quad (3)$$

The boundary conditions are given as

$$\lambda u = \mu_f \frac{\partial u}{\partial y}, V = V_w, -k_f \frac{\partial T}{\partial y} = h_f (T_f - T)$$

At  $y = 0$  (4)

$$u = u_\infty, T = T_\infty, \text{ at } y = \infty$$

Where  $u$  and  $v$  are the velocity components along the  $x$  and  $y$  directions respectively,  $T_f$  is temperature,  $T_\infty$  is the free stream temperature,  $u_\infty = ax$  is the free stream velocity which implies that the free stream velocity is increasing with axial distance along the plate surface,  $\rho$  is the density,  $\alpha = k/(\rho C_p)_f$  is the thermal diffusivity,  $k$  is the thermal conductivity,  $\nu = \mu/\rho_f$  is the kinematic viscosity coefficient,  $\mu$  is the dynamic viscosity,  $C_p$  is the specific heat at constant pressure,  $\sigma$  is the electrical conductivity.

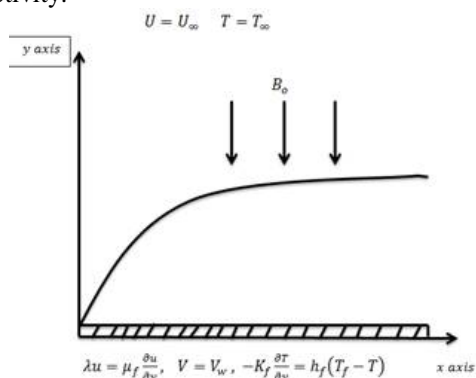


Fig. 1. Schematic Diagram of Flow

Using the Roseland approximation for the thermal radiation [15], the radiative heat flux is simplified as;

$$q_r = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial y} \quad (5)$$

Where  $\sigma^*$  is the Stephan-Boltzmann and  $k^*$  is the mean absorption coefficient.

The temperature differences within the flow are assumed to be sufficiently small such that  $T^4$  may be expressed as a linear function of temperature  $T$ . This is

done by expanding  $T^4$  in a Taylor series about a free stream temperature  $T_\infty$  as shown below;

$$T^4 = T_\infty^4 + 4T_\infty^3(T - T_\infty) + 6T_\infty^2(T - T_\infty)^2 \pm \dots$$

If we neglect higher order terms in the above equation beyond the first degree of  $(T - T_\infty)$ , we get

$$T^4 \approx 4T_\infty^3 T - 3T_\infty^4 \quad (6)$$

Substitute equation (4.6) into equation (4.5), we get

$$q_r = -\frac{16T_\infty^3 \sigma^*}{3k^*} \frac{\partial T}{\partial y} \quad (7)$$

Using the boundary layer approximations and introducing equation (4.7), the governing equations become;

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (8)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = U_\infty \frac{\partial u_\infty}{\partial x} + \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2 (U - U_\infty)^2}{\rho_f} \quad (9)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2} + \frac{\mu}{(\rho C_p)_f} \left[ \frac{\partial u}{\partial y} \right]^2 + \frac{\sigma B_0^2 (U - U_\infty)^2}{(\rho C_p)_f} - \frac{16\sigma^* T_\infty^3}{3k} \frac{\partial^2 T}{\partial y^2} \quad (10)$$

Using the stream function  $\psi = \psi(x, y)$  the velocity components  $u$  and  $v$  are defined as;

$$u = \frac{\partial \psi}{\partial y} \text{ and } v = -\frac{\partial \psi}{\partial x} \quad (11)$$

By means of similarity transformations, the dimensionless variables are defined as

$$\eta = (a/v_f)^{1/2} y, \psi = (av_f)^{1/2} \theta(\eta), \theta(\eta) = \frac{T - T_\infty}{T_f - T_\infty} \quad (12)$$

The governing equations (8), (9), and (10) combined with the boundary equations are transformed into ordinary differential equations as follows:

$$f''' + ff' - (f')^2 + 1 - M(f' - 1) = 0 \quad (13)$$

$$\frac{1}{Pr} (1 + \frac{4}{3} R) \theta'' + f \theta' + Ec f'^2 + Ha Ec (f' - 1)^2 = 0 \quad (14)$$

The corresponding boundary conditions are:

$$f'(0) = \beta f''(0), f(0) = f_w, \theta' = Bi[\theta - 1], \quad f'(\infty) = 1, \theta(\infty) = 0 \quad (15)$$

$f'$  and  $\theta$  are the dimensionless velocity and temperature respectively.  $Pr$ ,  $R$ ,  $Ec$  and  $Ha$  denote Prandtl number, Radiation parameter, Eckert number and the Hartmann number also known as the magnetic parameter respectively

They are defined as

$$Pr = \frac{\nu}{\alpha}, R = \frac{4\sigma^* T_\infty^3}{k^* k}, Ec = \frac{v_f^2}{C_p (T_f - T_\infty)}, Ha = \frac{\sigma B_0^2}{\rho_f a} \quad (16)$$

The physical quantities of practical significance in this dissertation are skin friction coefficient and Nusselt number. The skin friction coefficient  $C_f$  and the local Nusselt number  $Nu_x$  are expressed as:

$$C_f = \frac{\tau_w}{\rho_f U_\infty^2} \quad Nu = \frac{x q_w}{k_f (T_f - T_\infty)} \quad (17)$$

Where  $\tau_w$  is the wall shear stress and  $q_w$  is the heat flux from the plate. They are defined as:

$$\tau_w = \mu \frac{\delta u}{\delta y} \text{ as } y = 0 \text{ and } q_w = -k \frac{\delta T}{\delta y} \text{ as } y = 0 \quad (18)$$

From above we get that

$$\text{Re}_x^{1/2} C_f = f''(0) \text{ and } \text{Nur} = \text{Re}_x^{-1/2} Nu_x = -\theta'(0) \text{ Where}$$

$C_f$  is the local skin friction

$\text{Nur}$  is the reduced Nusselt number

$\text{Re}_x$  is the local Reynolds number

### III. SOLUTION OF THE PROBLEM

The set of non-linear differential equations (13) and (14) with the boundary conditions (15) were solved numerically using Runge-Kutta fourth order algorithm with a systematic guessing of shooting technique until the boundary condition at infinity were satisfied. The computation was done by a computer programme which uses a symbolic and computational language Maple. Numerical computations were performed for various values of the physical parameters involved. Namely; Magnetic parameter  $M$  (Hartmann number  $Ha$ ), Prandtl number  $\text{Pr}$  and Eckert number  $Ec$ . For illustration of the results, numerical values were plotted in figures 2 to 9 and a detailed discussion on the effects of the governing physical parameters on the velocity profile, temperature profile and skin friction coefficient was later done. The Prandtl number of the based fluid (water) was kept constant at 6.2.

### IV. RESULTS AND DISCUSSION

#### 4.1 Effect of Parameter Variation on the Velocity Profile

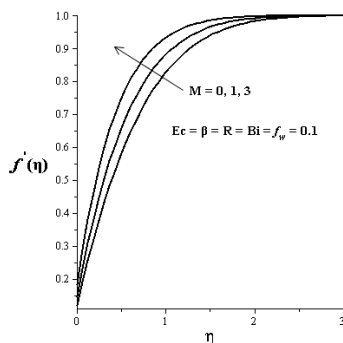


Fig. 2. Velocity profile against  $\eta$  with increasing Magnetic field intensity

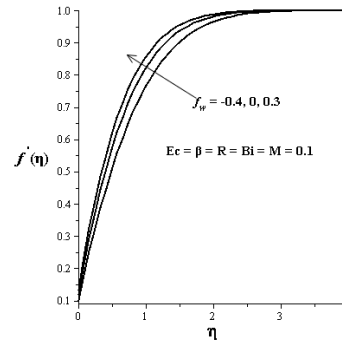


Fig. 3. Velocity profile against  $\eta$  with increasing suction/injection parameter

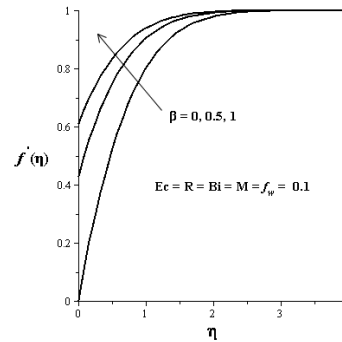


Fig. 4. Velocity profile with increasing Slip Parameter

Fig. 2 above shows the effects of different values of the magnetic parameter ( $M=0, 1, 3$ ) on the velocity profile. It shows that velocity increases with increasing values of  $M$ . It is also noted that the thickness of the momentum boundary layer decreases. This is as a result of the Lorentz force which arises from the interaction of magnetic and electric fields during the motion of the electrically conducting fluid.

Fig. 3 above shows the effect of different values of the suction parameter  $f_w = -0.4, 0, 0.3$  on the velocity profile. It shows that for a fixed value of  $\eta$ , the velocity profile increases as the suction parameter increases and as a result the boundary layer thickness becomes thinner.

Fig. 4 above shows the effects of different values of the slip parameter on the velocity profile. It is noted that the velocity increases with increasing values of the slip parameter and the momentum boundary layer decreases and becomes thinner.

#### 4.2 Effect of parameter variation on the Temperature Profile

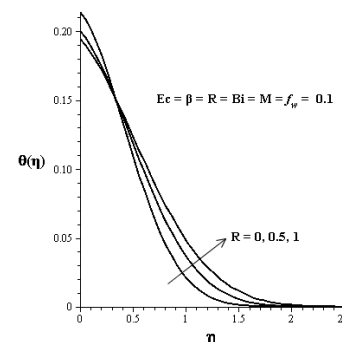


Fig. 5. Temperature profile with increasing Radiation parameter

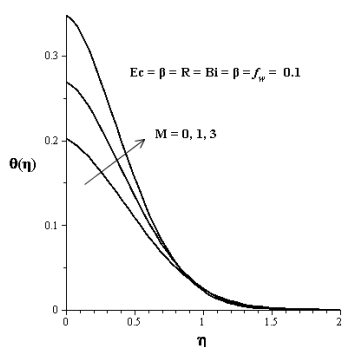


Fig. 6. Temperature profile with increasing Magnetic field intensity

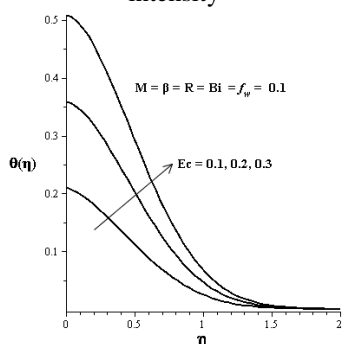


Fig. 7. Temperature profile with increasing Eckert number

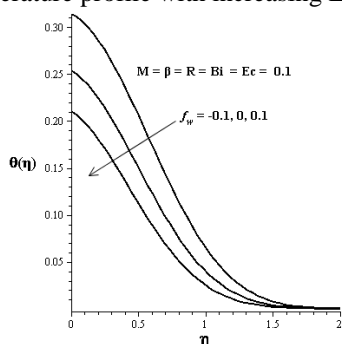


Fig. 8. Temperature profile with increasing Suction/injection parameter

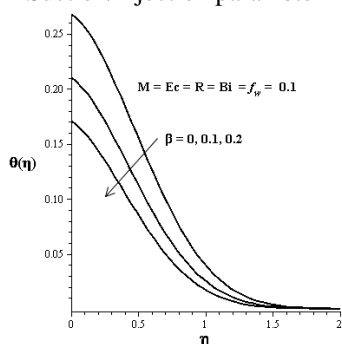


Fig. 9. Temperature profile with increasing Slip parameter

Fig. 5-9 above shows the effect of different parameters on the fluid temperature profile. It is noted that the temperature is maximum at the plate surface due to convective heating but decreases exponentially to zero far away from the plate surface satisfying the free stream conditions. Fig 4 shows the effect of the radiation parameter on the temperature profile. Figure 5 shows the effect of different values of  $M$  on the temperature distribution. It is noted that temperature decreases with increasing values of  $M$ . The temperature field for various values of Suction/Injection parameter  $f_w$  is shown in fig. 7. It is noted that for a fixed value of  $\eta$ , temperature decreases as  $f_w$  decreases. An increase in the Suction parameter means that more fluid is sucked through the permeable surface to the surrounding, hence a reduction in thermal boundary layer thickness is expected. Fig. 6 shows the effects of different values of Eckert number  $Ec$  on temperature. It is observed that for any fixed value of  $\eta$  temperature decreases as  $Ec$  increases. Fig 8 shows the effects of different values of the Slip parameter on the temperature profile.

#### 4.3 Effects of Parameters Variation on the Skin Friction and Nusselt Number.

$f_w$	$M$	$\beta$	$R$	$Ec$	$Bi$	$f''(0)$	$-\theta'(0)$
0	0.1	0.1	0.1	0.1	0.1	1.1651	0.0355
1						1.6531	0.0814
2						2.1632	0.08876
3						2.6541	0.0914
0.1	0					1.1809	0.0745
	1					1.4431	0.0630
	2					1.6469	0.0542
	5					1.8163	0.0468
		0				1.3301	0.0445
		1				1.6085	0.0922
		2				1.3812	0.0947
		3				0.2767	0.0953
			0			1.3301	0.0617
			1			1.3301	0.0693
			2			1.3301	0.0719
			3			1.3301	0.3784
				0		1.3301	0.0945
				0.1		1.3301	0.0724
				0.2		1.3301	0.0503
				0.3		1.3301	0.0281

Table 1 above shows the effect of various governing parameters on the Skin friction coefficient  $f''(0)$  and Nusselt number  $-\theta'(0)$ . It is seen that increasing  $f_w$ , increases both  $f''(0)$  and  $-\theta'(0)$ . An increase in  $M$  leads to an increase in  $f''(0)$  but decreases the Nusselt number  $-\theta'(0)$ . An increase in  $\beta$  reduces  $f''(0)$  but it increases  $-\theta'(0)$ . An increase in the Eckert number  $Ec$  has no effect on  $f''(0)$  but it reduces  $-\theta'(0)$ . An increase in  $R$  has no effect on  $f''(0)$  but it increases  $-\theta'(0)$ .

## V. CONCLUSION

From the study we have shown that it is true that a higher Prandtl number has the effect of having a relatively lower thermal conductivity in a fluid which reduces conduction and thereby increasing heat transfer rate at the surface. The Prandtl number controls the relative thickness of the momentum and thermal boundary layers. When Prandtl number is small, it means that the heat diffuses quickly compared to the velocity (momentum). This means that for liquid metals the thickness of the thermal boundary layer is much bigger than the velocity boundary layer.

### Abbreviations and Acronyms

$(u, v)$	Velocity components
$(x, y)$	Coordinates
$B_0$	Constant applied magnetic field
$C_p$	Specific heat at constant pressure
$Nu$	Local Nusselt number
$Pr$	Prandtl number
$Ec$	Eckert number
$M$	Magnetic parameter
$q_w$	Dimensional heat flux
$Re_x$	Local Reynolds number
$T$	Temperature
$T_\infty$	Free stream temperature
$U_\infty$	Free stream velocity
$f_w$	Suction/Injection parameter
$k$	Thermal conductivity
$h_f$	Heat transfer coefficient
$T_w$	Skin friction or shear stress

### Greek symbols

$\psi$	Stream function
$\theta$	Dimensionless temperature
$\eta$	Similarity variable
$\beta$	Thermal expansion coefficient
$\alpha$	Thermal diffusivity
$\phi$	Solid volume fraction
$\mu$	Dynamic viscosity
$\nu$	Kinematic viscosity
$\rho$	Density
$\lambda$	Slip coefficient

### Subscripts

$f$	fluid
$s$	solid

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## AUTHOR'S PROFILE



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### Winifred Nduku Mutuku

Winifred Nduku Mutuku joined Kenyatta University and pursued Bachelor of Education (Science) from 1992 to 1996, graduating with First class honors (Cum Laude). She later joined a middle level college and pursued an International Diploma in Computer Science from 1999 to 2000. In 2005 she joined Kenyatta University for Msc Applied Mathematics and graduated in the year 2007 with a project in Computational Fluid Dynamics. From 2011 to 2014, Winifred was at Cape Peninsula University of Technology in South Africa studying for her Doctorate in Philosophy in Applied Mathematics. She graduated in the year 2014 with a Thesis titled "Analysis of Hydro magnetic Boundary layer flow and Heat Transfer of Nanofluids. She has widely published in International Journals, has participated and presented papers in several International conferences and Workshops. She has supervised and still is supervising students for Msc and PhD. She has previously held position as a Chairperson for African Women in Mathematics Association (AMWA-Kenya) and is currently the Vice-Secretary for the same Association. Currently she works as a Lecturer in the Department of Pure and Applied Mathematics at Kenyatta University. She also works as a Volunteer tutor and mentor.